

Code No: 156BC

**JAWAHARLAL NEHRU TECHNOLOGICAL UNIVERSITY HYDERABAD****B. Tech III Year II Semester Examinations, February/March - 2022****HEAT TRANSFER****(Mechanical Engineering)****Time: 3 hours****Max. Marks: 75****Answer any five questions  
All questions carry equal marks**

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- 1.a) Derive steady state general Heat conduction equation without heat generation in cylindrical systems.
- b) Write down the equation for conduction of heat through a slab or Plane wall. [10+5]
- 2.a) List the assumptions made while analyzing the heat flow from a finned surface.
- b) A 2cm thick steel slab heated to  $525^{\circ}\text{C}$  is held in air stream having a mean temperature of  $25^{\circ}\text{C}$ . Estimate the time interval when the slab temperature would not depart from the mean value of  $25^{\circ}\text{C}$  by more than  $0.5^{\circ}\text{C}$  at any point in the slab. The steel plate has the following thermos-physical properties:  $\rho = 7950 \text{ kg/m}^3$ ,  $c_p = 455 \text{ J/kg}^{\circ}\text{C}$ ,  $k = 46 \text{ W/m}^{\circ}\text{C.h}$  (heat transfer coefficient on plate surface) =  $36 \text{ W/m}^2\text{-}^{\circ}\text{C}$ . [5+10]
- 3.a) What are repeating variables and how are they selected for dimensional analysis?
- b) 3000 kg of water is heated per hour from  $30^{\circ}\text{C}$  to  $70^{\circ}\text{C}$  by pumping it through a certain heated section of a 25 mm diameter tube. If the surface of the heated section is maintained at  $110^{\circ}\text{C}$ , estimate length of the heated section and the rate of heat transfer from the tube to water. [5+10]
- 4.a) Derive an expression for LMTD for a Parallel Flow Heat Exchangers.
- b) A hot square plate of  $75 \text{ cm} \times 75 \text{ cm}$  at  $120^{\circ}\text{C}$  is exposed to atmospheric air at  $40^{\circ}\text{C}$ . Find the heat lost from both surfaces of the plate if it is kept in vertical position. [8+7]
- 5.a) Water is boiled at atmospheric pressure by a horizontal polished copper heating element of diameter  $D = 5 \text{ mm}$  and emissivity  $\epsilon = 0.05$  immersed in water. If the surface temperature of the heating wire is  $350^{\circ}\text{C}$ , determine the rate of heat transfer from the wire to the water per unit length of the wire.
- b) State and explain the Stefan-Boltzmann law of radiation heat transfer, giving the nomenclature involved in it. [8+7]
- 6.a) It is required to heat the oil to  $300^{\circ}\text{C}$  for frying purpose. A long ladle is used in frying pan. The section of the ladle is  $5 \text{ mm} \times 18 \text{ mm}$ . The surrounding air is at  $30^{\circ}\text{C}$  and the thermal conductivity of the ladle material is  $205 \text{ W/mK}$ . If the temperature at a distance of 380 mm from the oil should not exceed  $40^{\circ}\text{C}$ , determine convective heat transfer coefficient.
- b) Derive an expression for temperature distribution under steady state in one dimensional heat conduction for a plane wall. [8+7]

7. An electrically heated thin foil of length  $L = 25\text{ mm}$  and width  $W = 8\text{ mm}$  is to be used as a wind speed meter. Wind with a temperature  $T_\infty$  and velocity  $U_\infty$  blows parallel to the longest side. The foil is internally heated by an electric heater dissipating  $Q$  (Watts) from both sides and is to be operated in air with  $T_\infty = 20^\circ\text{C}$ ,  $C_p = 1.005\text{ kJ/kg K}$ ,  $\nu = 1.522 \times 10^{-5}\text{ m}^2/\text{s}$ ,  $\rho = 1.19\text{ kg/m}^3$  and  $Pr = 0.72$ . The surface temperature,  $T_s$  of the foil is to be measured at the trailing edge - but can be assumed to be constant. Estimate the wind speed when  $T_s = 32^\circ\text{C}$  and  $Q = 0.5\text{ W}$ . [15]

8.a) How heat exchangers are classified.

b) A double-pipe (shell-and-tube) heat exchanger is constructed of a stainless steel ( $k = 15.1\text{ W/m}^\circ\text{C}$ ) inner tube of inner diameter  $D = 1.5\text{ cm}$  and outer diameter  $D_o = 1.9\text{ cm}$  and an outer shell of inner diameter  $3.2\text{ cm}$ . The convection heat transfer coefficient is given to be  $h_i = 800\text{ W/m}^2^\circ\text{C}$  on the inner surface of the tube and  $h_o = 1200\text{ W/m}^2^\circ\text{C}$  on the outer surface. For a fouling factor of  $R_{fi} = 0.0004\text{ m}^2^\circ\text{C/W}$  on the tube side and  $R_{fo} = 0.0001\text{ m}^2^\circ\text{C/W}$  on the shell side, determine:

i) The thermal resistance of the heat exchanger per unit length.

ii) The overall heat transfer coefficients,  $U_i$  and  $U_o$  based on the inner and outer surface areas of the tube, respectively. [5+10]

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